

whereby said hydrogen atoms react with said catalyst in said vessel at a pressure less than atmospheric, thereby releasing energy and producing hydrogen atoms having a binding energy of about $E_b = 13.6/n^2$ eV, where n is a fraction whose numerator is 1 and denominator is an integer greater than 1.

53. A cell according to claim 52, wherein said gaseous catalyst comprises hydrogen atoms having a binding energy of about $E_b = 13.6/n^2$ eV, where n is a fraction whose numerator is 1 and denominator is an integer greater than 1.

54. A cell according to claim 52, wherein said cell maintains the reaction,

$$m \times 27.21 \text{ eV} + H \left[\frac{a_H}{m'} \right] + H \left[\frac{a_H}{p} \right] - H^+ + e^- + H \left[\frac{a_H}{(p+m)} \right] + [(p+m)^2 - p^2 - (m^2 - 2m)] \times 13.6 \text{ eV}$$

$$H^+ + e^- - H \left[\frac{a_H}{1} \right] + 13.6 \text{ eV}$$

$$H \left[\frac{a_H}{m'} \right] + H \left[\frac{a_H}{p} \right] - H \left[\frac{a_H}{1} \right] + H \left[\frac{a_H}{(p+m)} \right] + [2pm + m^2 - m'^2] \times 13.6 \text{ eV} + 13.6 \text{ eV}$$

where m and p are positive non-zero integers, m' is an integer greater than 1, and a_H is the radius of the hydrogen atom ($n=1$).

55. A cell according to claim 52, whereby said gaseous hydrogen atoms are formed in the cell by reacting molecules containing hydrogen atoms, and

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a second catalyst for disassociating said molecules to produce hydrogen atoms.

56. A cell according to claim 55, wherein said second catalyst is at least one element selected from the group consisting of transition elements and lanthanides.

sub 57 4 A cell according to claim 55, wherein said second catalyst is at least one element selected from the group consisting of the refractory metals, activated charcoal, platinum, palladium, gold, rhenium and iridium.

sub 58 4 A cell according to claim 55, further comprising a valve for controlling the flow of said molecules over said second catalyst.

sub 59 4 A cell according to claim 52, wherein said gaseous catalyst is adapted to sublime, boil, or volatilize when heated.

sub 60 4 A cell according to claim 52, wherein said gaseous catalyst is formed from a salt.

sub 61 4 A cell according to claim 60, wherein said salt is selected from the group consisting of halides, sulfates, phosphates, carbonates, hydroxides, and sulfides.

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62. A cell according to claim 60, wherein said gaseous catalyst is formed from a salt of rubidium or potassium.

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63. A cell according to claim 62, wherein said salt of potassium is selected from the group consisting of KF, KCl, KBr, KI, K₂S₂, KOH, K₂SO₄, K₂CO₃, K₂PO₄, and K₂GeF₄.

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64. A cell according to claim 62, wherein said salt of rubidium is selected from the group consisting of RbF, RbCl, RbBr, RbI, Rb₂S₂, RbOH, Rb₂SO₄, Rb₂CO₃, and Rb₃PO₄.

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65. A cell according to claim 52, wherein said gaseous catalyst comprises a cation having a vapor pressure greater than zero when said gaseous catalyst is heated, said cation being selected from the group consisting of (K⁺), (Rb⁺), (Mo²⁺), and (Ti²⁺).

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66. A cell according to claim 52, wherein said gaseous catalyst comprises a pair of cations having a vapor pressure greater than zero when said gaseous catalyst is heated, said pair of cations being selected from the group consisting of: (Sn⁴⁺, Si⁴⁺), (Pr³⁺, Ca²⁺), (Sr²⁺, Cr²⁺), (Cr³⁺, Tb³⁺), (Sb³⁺, Co²⁺), (Bi³⁺, Ni²⁺), (Pd²⁺, In⁺), (La³⁺, Dy³⁺), (La³⁺, Ho³⁺), (K⁺, K⁺), (V³⁺, Pd²⁺), (Lu³⁺, Zn²⁺), (As³⁺, Ho³⁺), (Mo⁵⁺, Sn⁴⁺), (Sb³⁺, Cd²⁺), (Ag²⁺, Ag⁺), (La³⁺, Er³⁺), (V⁴⁺, B³⁺), (Fe³⁺, Ti³⁺), (Co²⁺, Ti⁺), (Bi³⁺, Zn²⁺), (As³⁺, Dy³⁺), (Ho³⁺, Mg²⁺), (K⁺, Rb⁺), (Cr³⁺, Pr³⁺), (Sr²⁺, Fe²⁺), (Ni²⁺, Cu⁺), (Sr²⁺, Mo²⁺),

(Y³⁺, Zr⁴⁺), (Cd²⁺, Ba²⁺), (Ho³⁺, Pb²⁺), (Pd²⁺, Li⁺), (Eu³⁺, Mg²⁺), (Er³⁺, Mg²⁺), (Bi⁴⁺, Al³⁺), (Ca²⁺, Sm³⁺), (V³⁺, La³⁺), (Gd³⁺, Cr²⁺), (Mn²⁺, Tl⁺), (Yb³⁺, Fe²⁺), (Ni²⁺, Ag⁺), (Zn²⁺, Yb²⁺), (Se⁴⁺, Sn⁴⁺), (Sb³⁺, Bi²⁺), and (Eu³⁺, Pb²⁺).

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67. A cell according to claim 52, wherein said gaseous catalyst comprises an ionic compound resistant to reduction by hydrogen atoms.

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68. A cell according to claim 52, wherein said gaseous catalyst is adapted to provide ions.

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69. A cell according to claim 52, whereby said vessel maintains a hydrogen partial pressure of less than about one torr.

70. A cell according to claim 52, wherein said vessel maintains said catalyst in molten form.

71. A cell according to claim 52, wherein the temperature of said vessel is maintained at about 50 °C above the melting point of said gaseous catalyst.

72. A cell according to claim 52, wherein the hydrogen partial pressure in said vessel is maintained at about 200 millitorr.

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73. A cell according to claim 66, wherein the temperature of said vessel is maintained at about 50 °C above the higher melting point of compounds of the two cations comprising said cation pair of said gaseous catalyst.

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74. *23* A cell according to claim 52, further comprising a valve for selectively releasing said catalyst from said vessel.

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75. *24* A cell according to claim 52, further comprising a valve for selectively releasing said hydrogen atoms having a binding energy of about $E_b = 13.6/n^2$ eV, where n is a fraction whose numerator is 1 and denominator is an integer greater than 1.

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76. A cell according to claim 52, wherein the vapor partial pressure of said gaseous catalyst varies with temperature.

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77. A cell according to claim 52, further comprising a heater for heating said vessel.

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78. A cell according to claim 52, further comprising a catalyst reservoir communicating with said reaction vessel, said catalyst reservoir containing said gaseous catalyst or a source thereof.

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79. A cell according to claim 78, further comprising a heater for heating said catalyst.

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80. A cell according to claim 78, wherein said catalyst reservoir is external to said reaction vessel.

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81. A cell according to claim 80, further comprising a flow control valve for controlling the flow of said catalyst from said catalyst reservoir into said vessel.

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82. A cell according to claim 52, further comprising a chamber for containing hydrogen atoms or a source of hydrogen atoms communicating with said reaction vessel.

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83. A cell according to claim 82, further comprising a flow control valve for controlling the flow of hydrogen atoms from said chamber into said vessel.

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84. A cell according to claim 82 wherein said source of hydrogen atoms comprises an internal combustion engine.

85. A cell according to claim 82, wherein said source of hydrogen atoms comprises a tungsten capillary heated to between 1800 and 2000 K for dissociating molecules containing hydrogen atoms to produce hydrogen atoms.

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86. A cell according to claim 85, further comprising a valve for controlling the flow of said molecules over said tungsten capillary.

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87. A cell according to claim 82, wherein said source of hydrogen atoms comprises an inductively coupled plasma flow tube for dissociating molecules containing hydrogen atoms to produce hydrogen atoms.

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88. A cell according to claim 87, further comprising a valve for controlling the flow of said molecules into said inductively coupled plasma flow tube.

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89. A cell according to claim 87, further comprising a power controller for controlling the power dissipated in said inductively coupled plasma flow tube.

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90. A cell according to claim 52, further comprising a heat exchanger for removing said extracted energy from said cell.

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91. A cell according to claim 52, further comprising a power gauge for measuring the amount of extracted ^{power} energy in said cell.

92. A method for extracting energy from hydrogen comprising the steps

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of:

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providing a gaseous catalyst having a net enthalpy of reaction of about $27 * (p/2)$ eV, where p is an integer greater than 1;

providing gaseous hydrogen atoms; and

reacting said gaseous catalyst with said gaseous hydrogen atoms, thereby producing hydrogen atoms having a binding energy of about $E_b = 13.6/n^2$ eV, where n is a fraction whose numerator is 1 and denominator is an integer greater than 1,

said reaction occurring at a pressure less than atmospheric pressure.

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93. A method according to claim 92, wherein said gaseous hydrogen atoms are provided by disassociating molecules containing hydrogen atoms.

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94. A method according to claim 92, wherein gaseous hydrogen atoms are provided by contacting molecules containing hydrogen atoms with a ~~catalyst~~ for *second catalyst* disassociating said molecules to produce hydrogen atoms in the gas phase.

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95. A method according to claim 92, wherein said gaseous catalyst comprises gaseous hydrogen atoms having a binding energy of about $E_b = 13.6/n^2$ eV, where n is a fraction whose numerator is 1 and denominator is an integer greater than 1.

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96. A method according to claim 92, wherein said gaseous catalyst is provided according to the reaction,

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$$m \times 27.21 \text{ eV} + H \left[\frac{a_H}{m'} \right] + H \left[\frac{a_H}{p} \right] - H^+ + e^- + H \left[\frac{a_H}{(p+m)} \right] + [(p+m)^2 - p^2 - (m^2 - 2m)] \times 13.6 \text{ eV}$$

$$H^+ + e^- \rightarrow H \left[\frac{a_H}{1} \right] + 13.6 \text{ eV}$$

$$H \left[\frac{a_H}{m'} \right] + H \left[\frac{a_H}{p} \right] - H \left[\frac{a_H}{1} \right] + H \left[\frac{a_H}{(p+m)} \right] + [2pm + m^2 - m^2] \times 13.6 \text{ eV} + 13.6 \text{ eV}$$

where m and p are positive non-zero integers, m' is an integer greater than 1, and a_H is the radius of the hydrogen atom ($n=1$).

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97. A method according to claim 92, wherein said gaseous catalyst is provided by volatilizing a material to a gaseous state and ionizing said gaseous material.

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98. A method according to claim 92, wherein said hydrogen atoms are provided by flowing gaseous molecules containing hydrogen atoms over a hot refractory metal, transition metal, platinum, palladium, gold, rhenium, or iridium.

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99. A method according to claim 92, wherein said hydrogen atoms are provided by flowing gaseous molecules containing hydrogen atoms over a tungsten capillary heated by electron bombardment to between 1800 and 2000 K.

100. A method according to claim 92, wherein said hydrogen atoms are provided by flowing gaseous molecules containing hydrogen atoms in an inductively coupled plasma flow tube.

101. A method according to claim 92, wherein said reaction occurs at a pressure less than about one torr.

102. A method according to claim 92, wherein the partial pressure of hydrogen atoms in the reaction is less than about one torr.

103. A method according to claim 92, wherein the partial pressure of hydrogen atoms in the reaction is about 200 millitorr.

104. A method according to claim 92, wherein the partial pressure of the gaseous catalyst in the reaction is between about 50 and 250 millitorr.

105. A method according to claim 92, wherein said reaction occurs at a temperature of about 50 °C above the melting point of said gaseous catalyst.

106. A method according to claim 92, wherein the vapor partial pressure of said gaseous catalyst is controlled by varying the temperature of said gaseous catalyst.